
Variation in Flame Surface Density in Acoustically Perturbed Flames

Albert Ratner

*Mechanical and Industrial Engineering
University of Iowa*

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University of Iowa



University of Iowa – Flood of June 2008



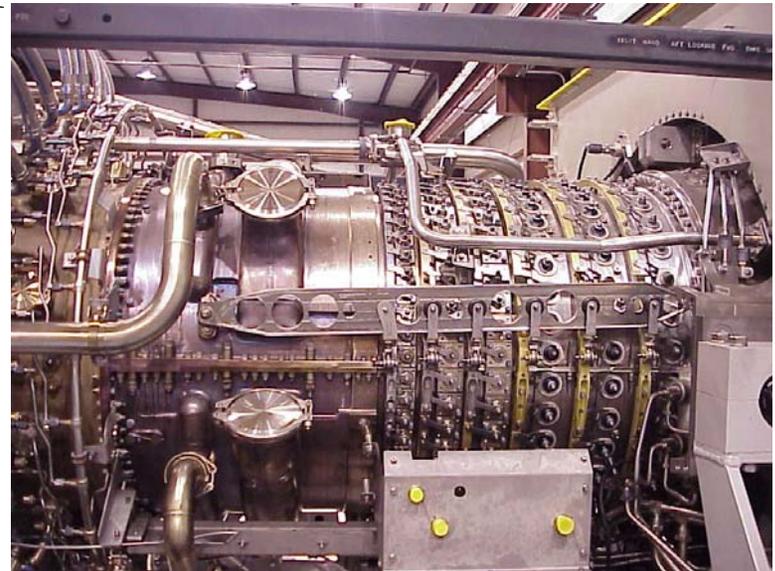
Outline

- Motivation – Why are we interested?
- Methodology – How is ours different?
- Experimental system
 - Chamber, burner, & imaging system
- Results and analysis
 - Flame Surface Density assessment
 - Analysis of physical mechanisms
- Conclusions



Motivation – Continuing Issues in Gas Turbine Power Systems

- ❑ Common problem: many combustion systems exhibit instabilities
- ❑ Instabilities may arise out of inadequate design or off-design operation
- ❑ Combustion instability is a result of interactions between system acoustics, system flow topology, and energy/heat release
- ❑ Instability can generate acoustic waves strong enough disturb the flow field, increase wall heat transfer, induce system vibration, and even catastrophic failure



Methodology

□ Objective

- *Examine the acoustics/ combustion interaction for lean premixed low swirl stabilized flames*
- Assess flame/flow coupling
- Observe changes in the relative importance of various effects as scaling parameters are varied

□ Technique

- Chamber-based (downstream of flame) acoustic driving
 - Minimizes the effect of mass/turbulence intensity oscillations at the burner exit...
- PLIF imaging:
 - Phase-resolved data acquisition followed by phase-dependent re-sorting...

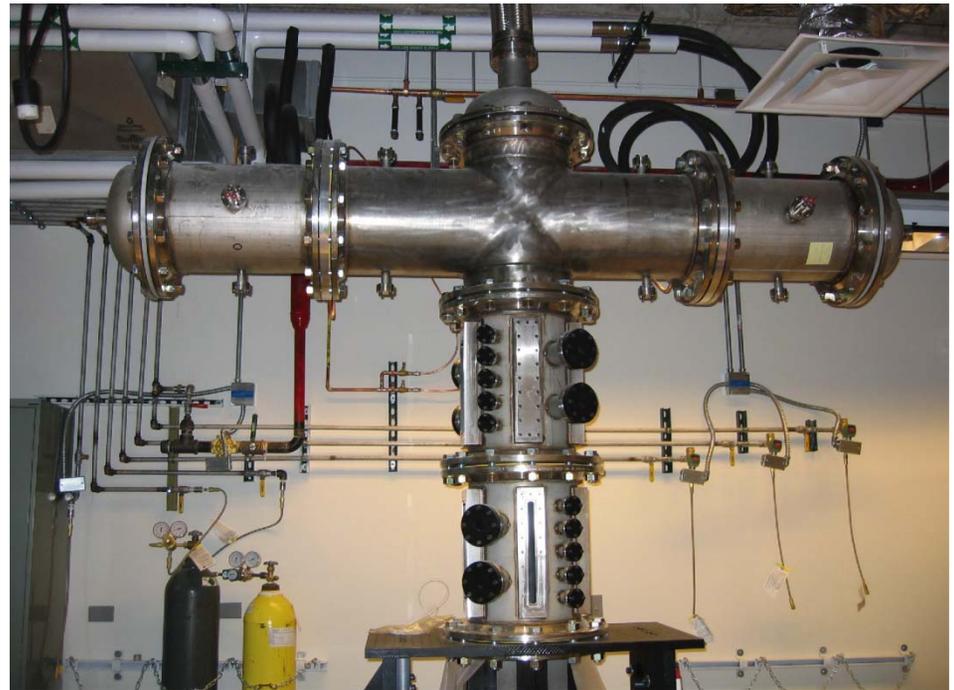
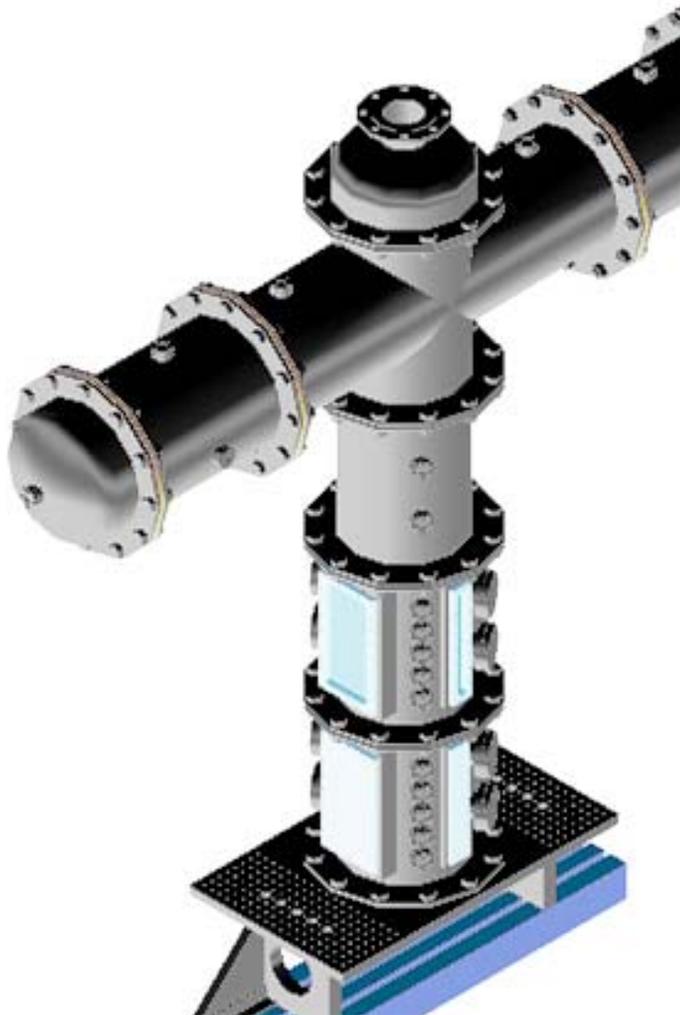


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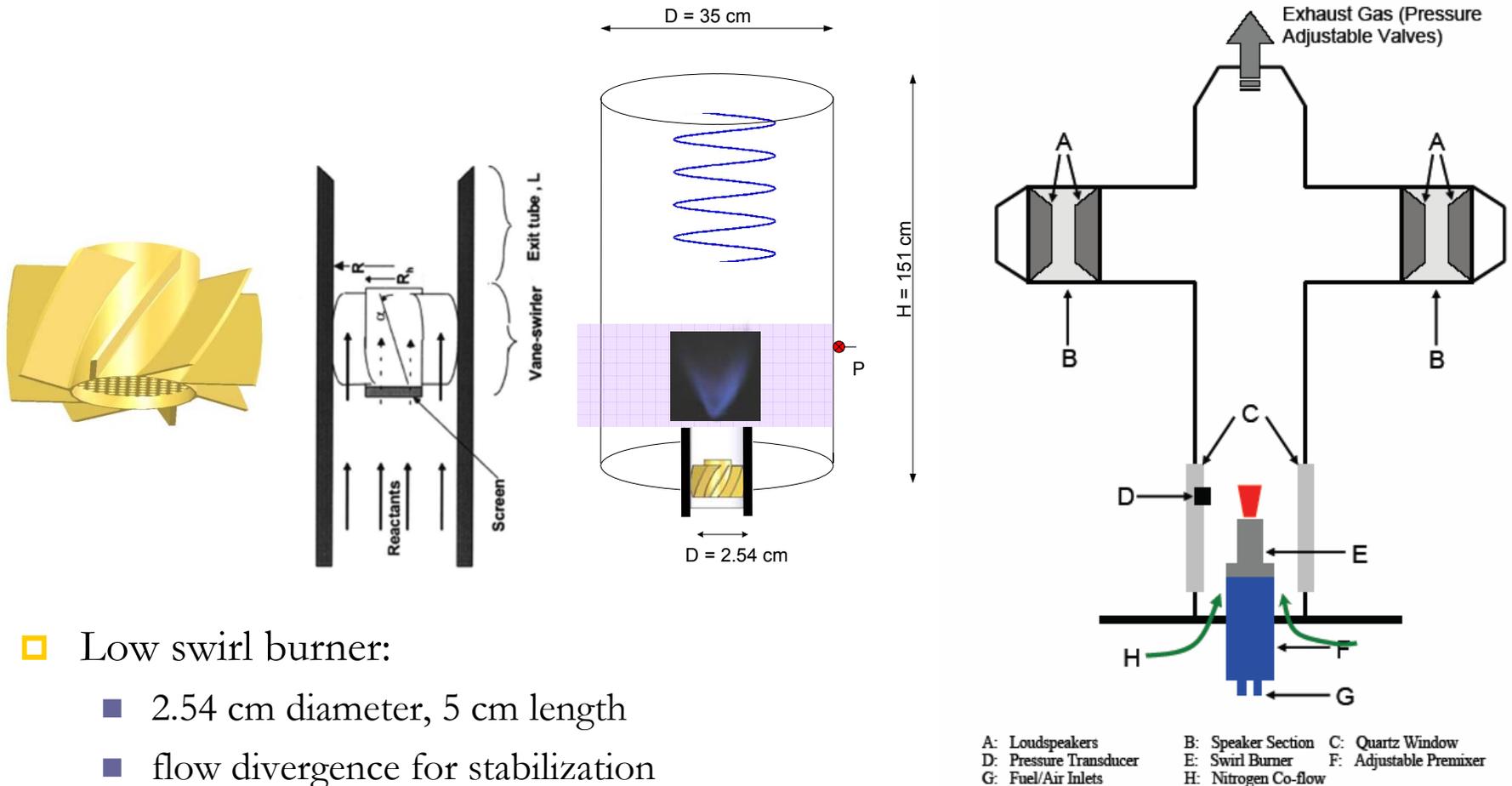
Experimental System - Chamber



- ▣ Stainless Steel Chamber
 - Diameter 12", height: 6'
- ▣ Optical imaging windows
- ▣ Side access ports



Experimental System – Chamber & Burner

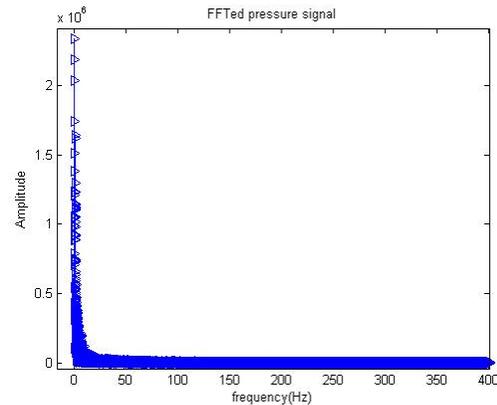
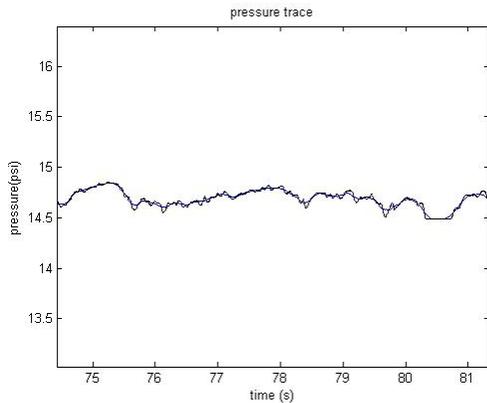


Low swirl burner:

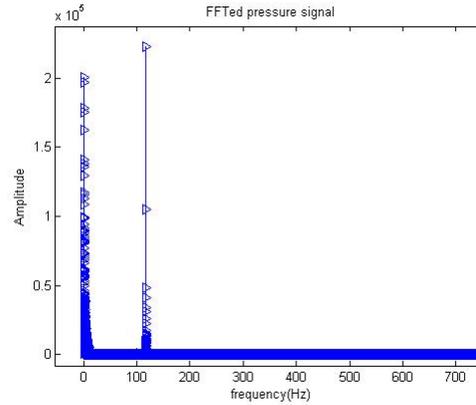
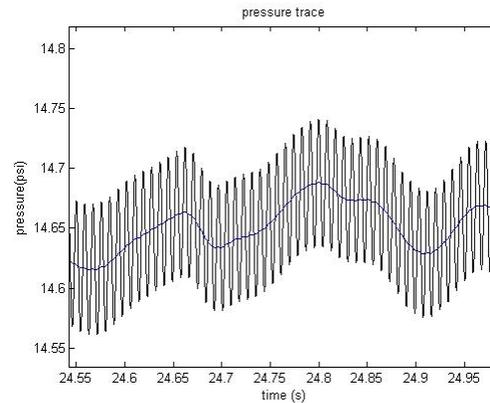
- 2.54 cm diameter, 5 cm length
- flow divergence for stabilization
- provided by Dr. Robert Cheng of LBNL



Pressure fluctuations

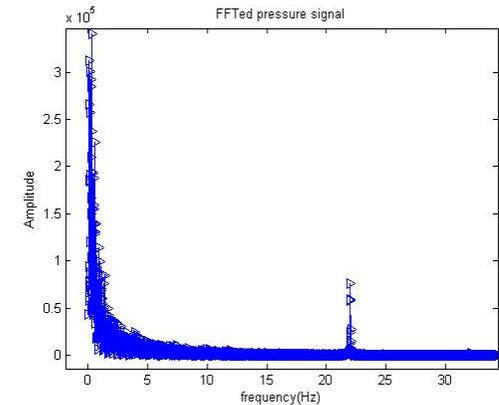
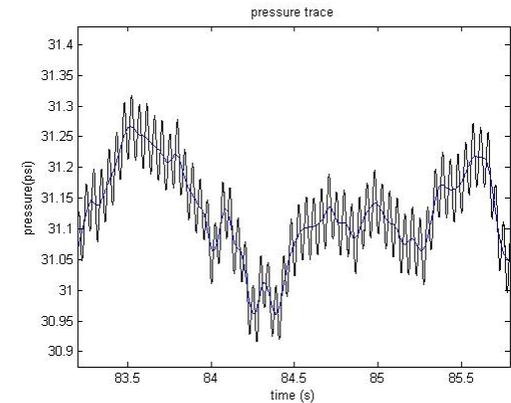


No excitation



$f=116$ Hz

pressure fluctuation at 1 bar



pressure fluctuation at 2 bar

- In general, P_{rms} is about 0.05%. But it also depends on excitation frequency



Experimental System - Imaging

□ Laser system

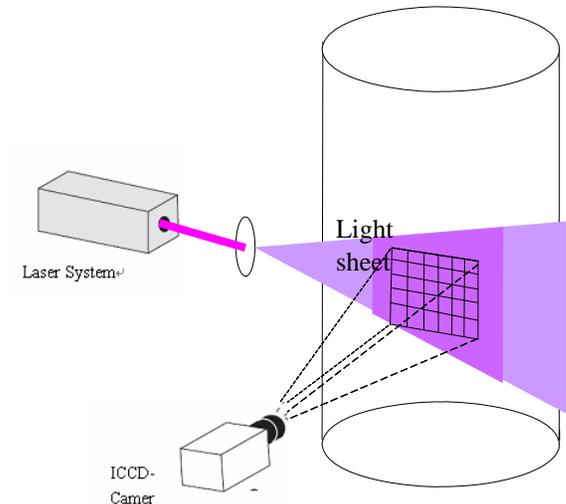
- Nd:YAG pump laser, dye laser, frequency doubler
- Sheet-forming optics

□ Camera system

- ICCD camera
- View field: 8.9cm*8.9cm (512*512)

□ Excitation – detection

- 283 nm pump beam with 308-350 nm detection



Simplified schematic view of imaging system



Experimental Conditions

□ Reactants

- fuel: methane
- oxidizer: air
- equivalence ratio: $\Phi=0.5$

□ Flow rates:

- air: 100 slpm, methane: 5 slpm
- reactants: 3.48m/s (outlet of the burner)

□ Enforced acoustics

- frequency: 22-370Hz
- amplitude: $\sim 0.05\%$

□ Chamber bulk pressure:

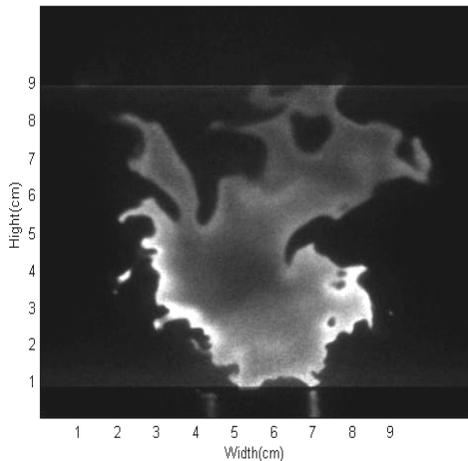
- $P= 1 - 5$ bar



OH-PLIF images

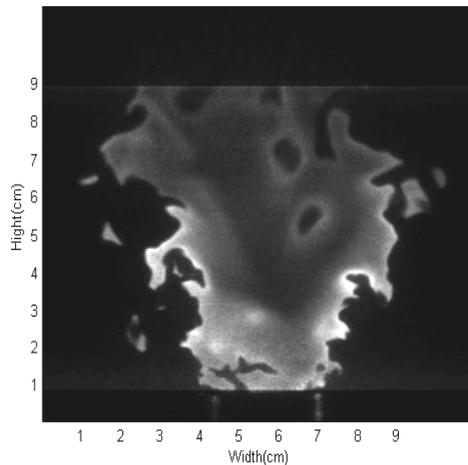
1 bar

instantaneous flame(OH-PLIF), $\phi = 0.59$, 1bar, 85Hz



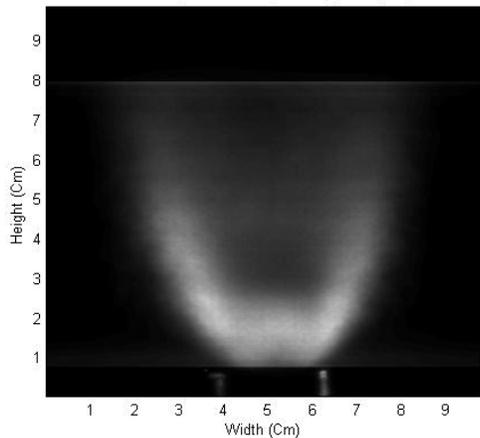
1.8 bar

instantaneous flame(OH-PLIF), $\phi = 0.59$, 1.8bar, 85Hz

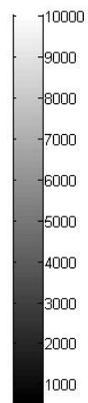
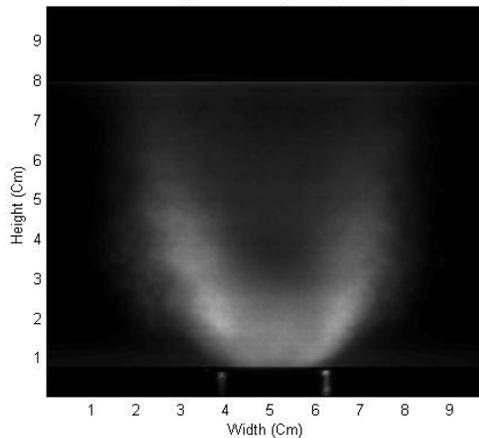


Instantaneous OH-PLIF images

Flame Intensity Distribution $\phi = 0.59$, $p = 14.7$ psi, 85Hz



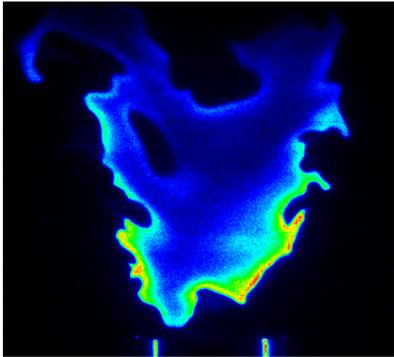
Flame Intensity Distribution $\phi = 0.59$, $p = 20$ psi, 85Hz



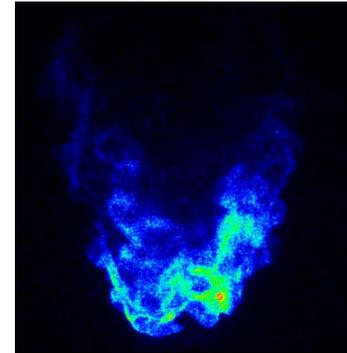
Mean OH-PLIF images



PLIF/Chemiluminescence Comparison



Instantaneous flame
from OH-PLIF

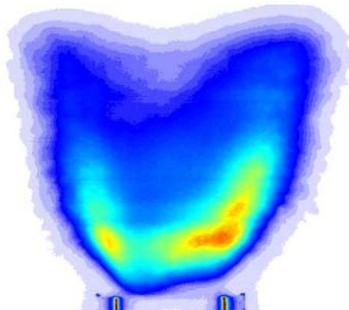


Instantaneous flame
from OH*

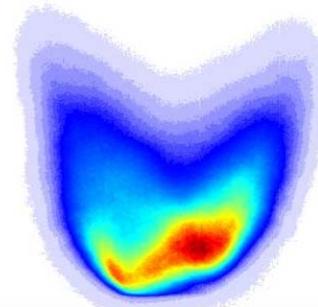


Visual image from ordinary camera

Averaged flame
from OH-PLIF



Averaged flame
from OH*

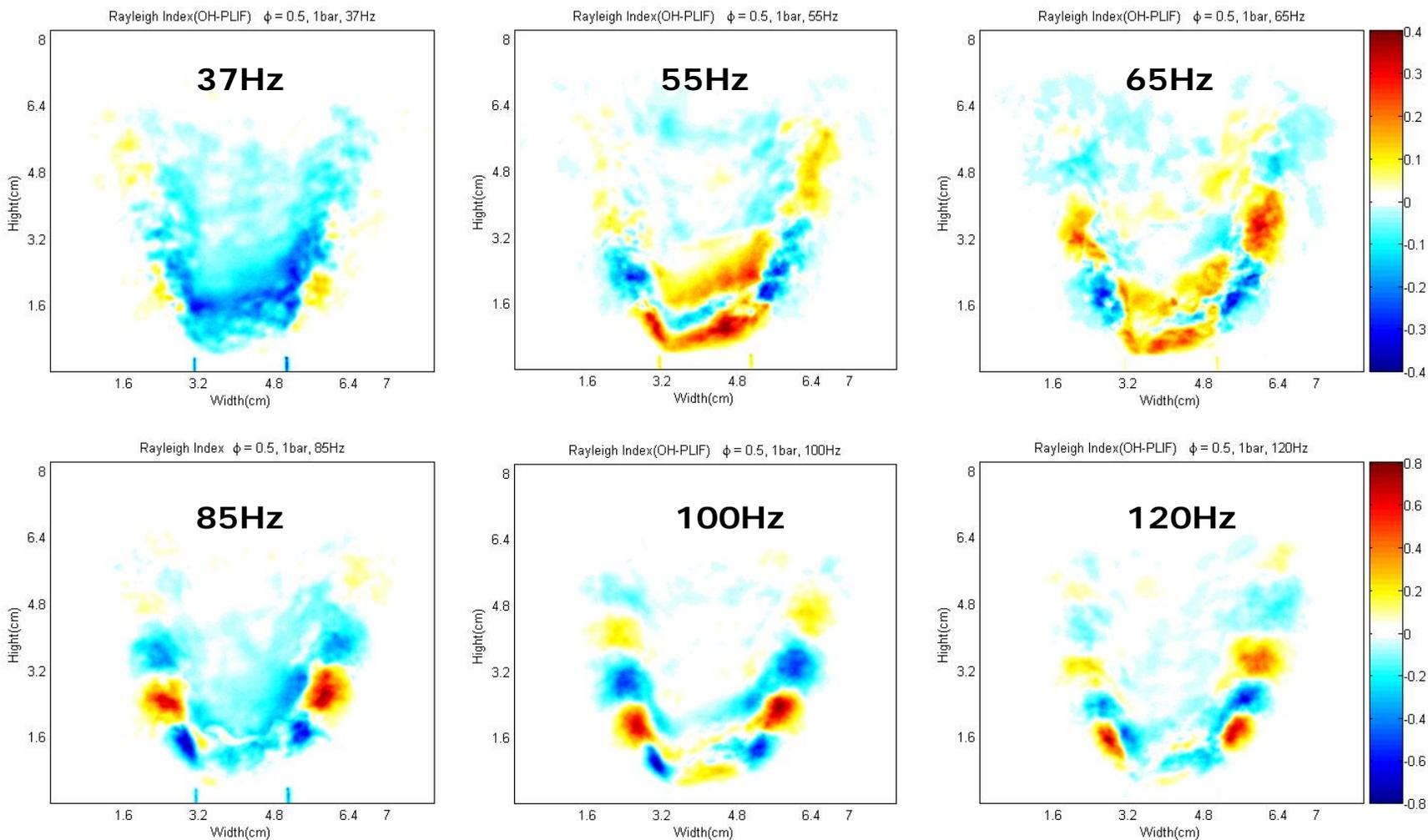


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Rayleigh Index Distribution from OH-PLIF

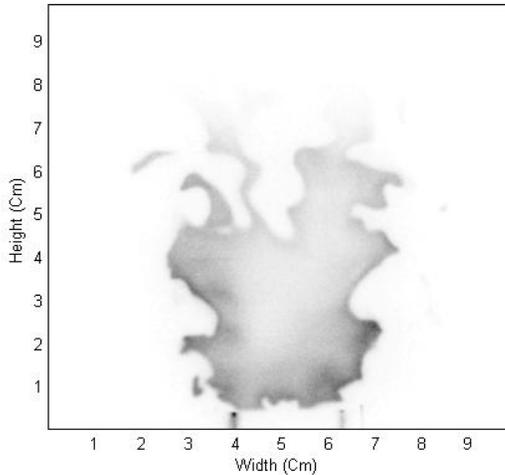


Rayleigh Index at the center plane of the flame

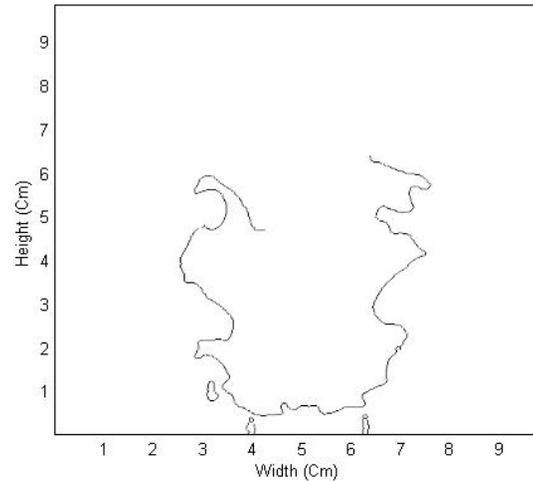


Flame Surface Density vs. Flame Intensity

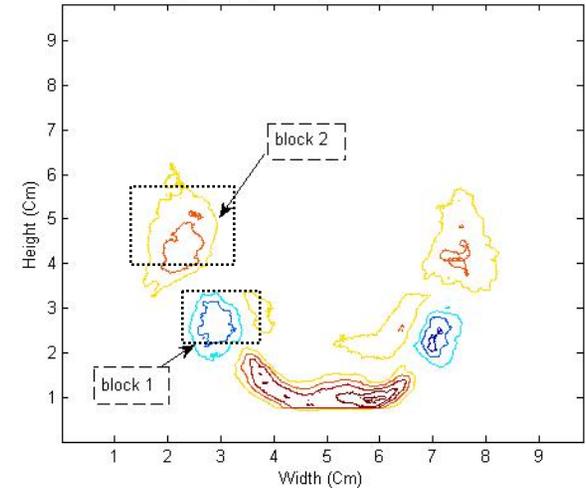
Instantaneous image



Flame front



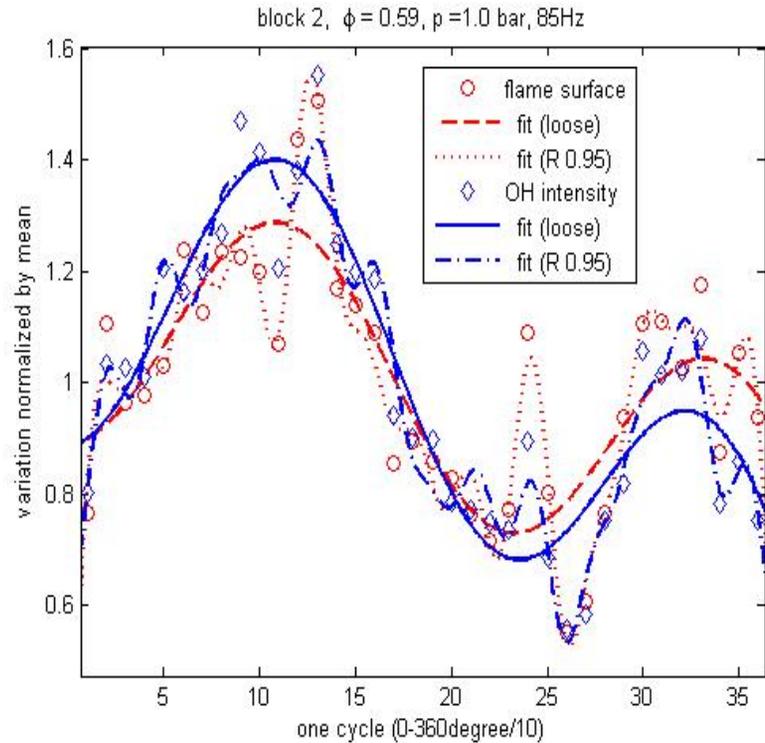
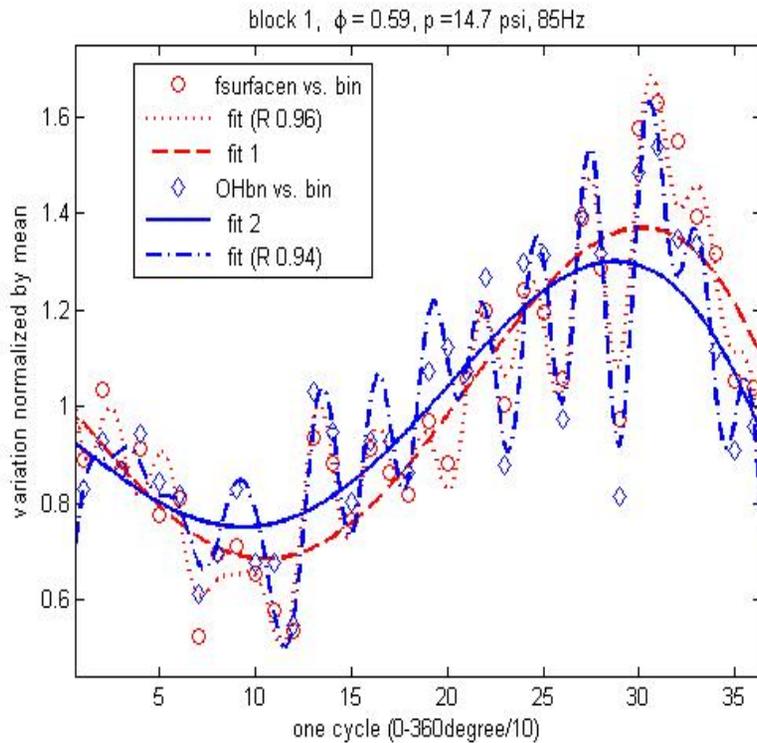
Averaged Rayleigh Index $\phi = 0.59$, $p = 1.0$ bar, 85Hz



- ❑ Flame surface density is approximated as: *total flame length/area*
- ❑ OH intensity is : *sum of OH/area*
- ❑ Calculated in Matlab



Flame Surface Density vs. Flame Intensity (1 bar)

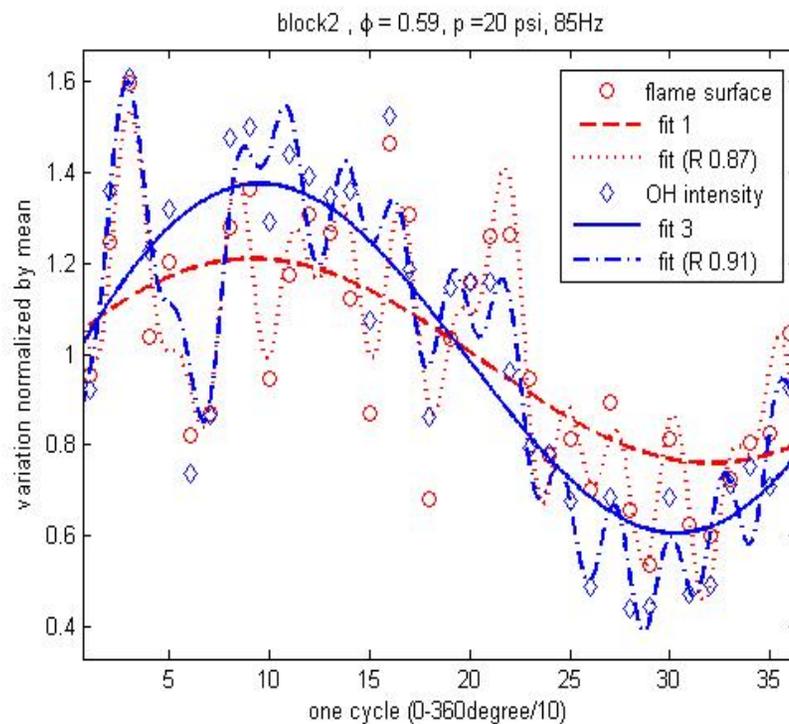
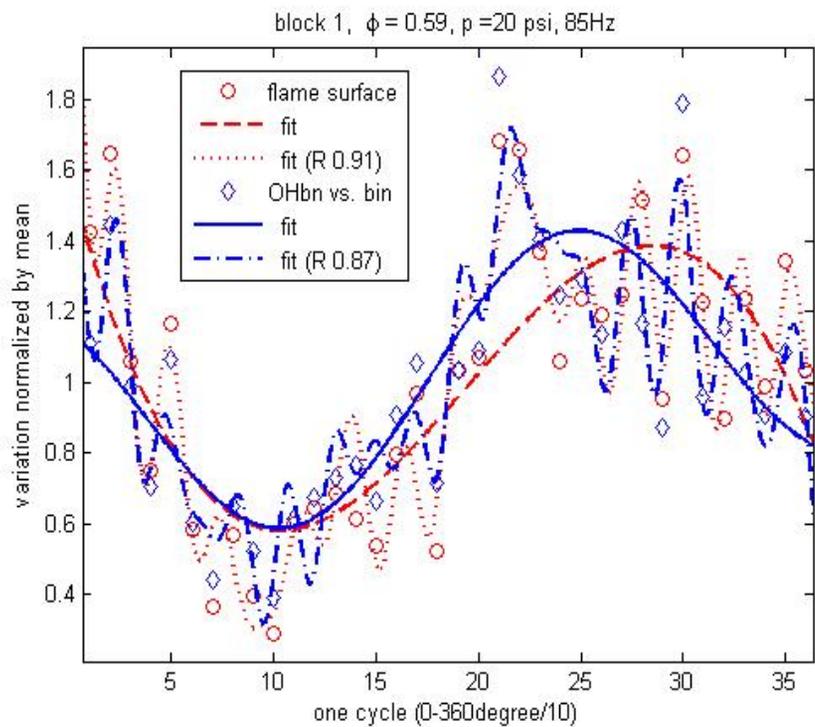


Correlation of FSD and OH at 1 bar

- Block 1: 0.94
- Block 2: 0.91



Flame Surface Density vs. Flame Intensity (1.5 bar)

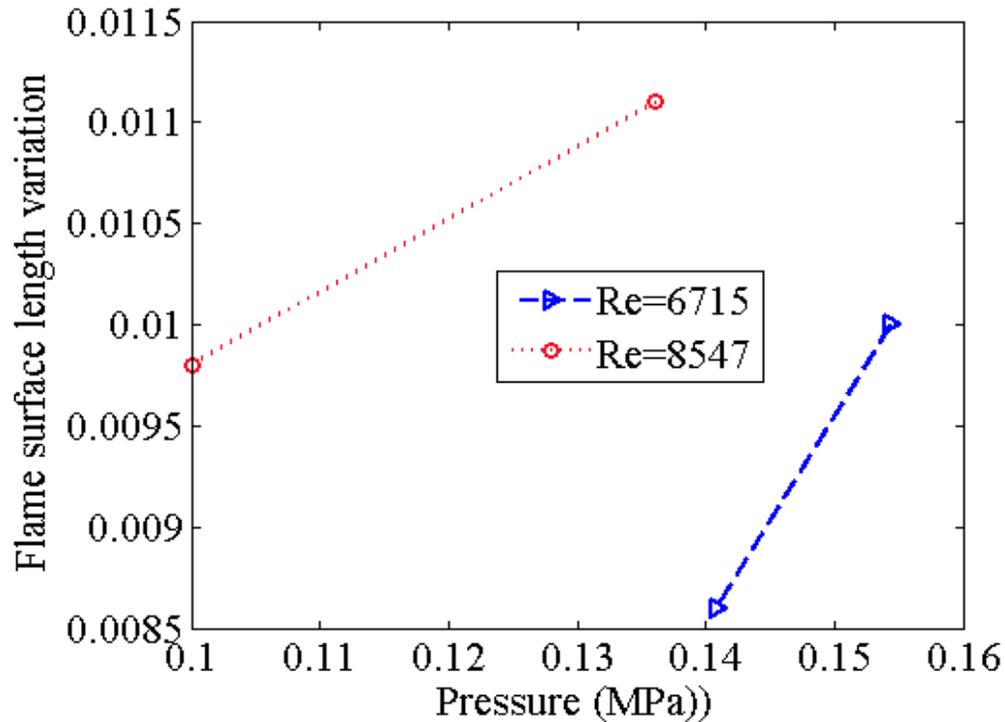


Correlation of FSD and OH at 1.5 bar

- Block 1: 0.92
- Block 2: 0.91



Flame Surface Density with Increasing Pressure



- ❑ Flame Surface Density increases with increasing pressure even while Reynolds number is held constant
- ❑ Increases are most likely due to increases in turbulence intensity



Natural Instability Growth

- Normal operation involves controlling the pressure amplitude by increasing or decreasing the driving power to hold the amplitude constant

- As a test, constant power was applied at various frequencies

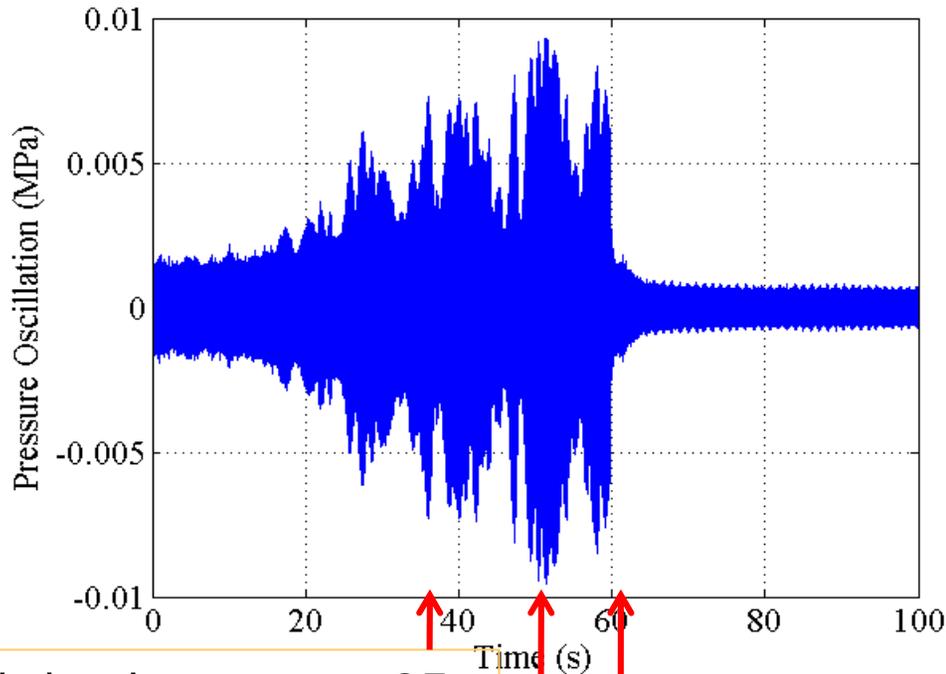
- At 125 Hz, the system slowly developed an unstable mode that grew the pressure amplitude, caused the flame to move upstream, and the flame to extinguish after some time

- It was found that there is a minimum driving pressure to establish the shear-layer vortex street that then can lead to this unstable mode



Effect of Pressure Oscillation Amplitude

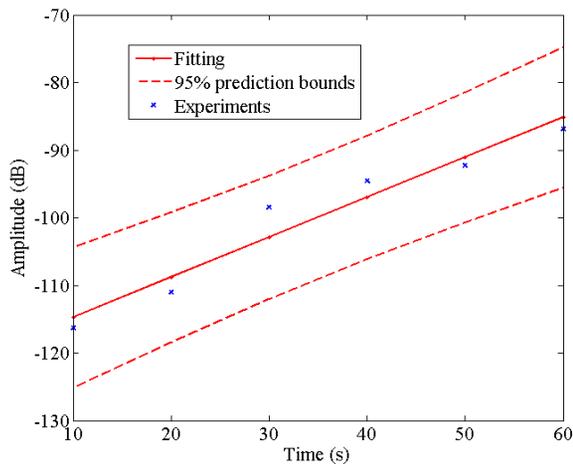
- The pressure variation p'/P has to be more than 0.04% to trigger coupling
- Between 0.04% to 0.7% perturbation, the distribution of the vortex structure remains unchanged
- Above 5%, flash back occurs



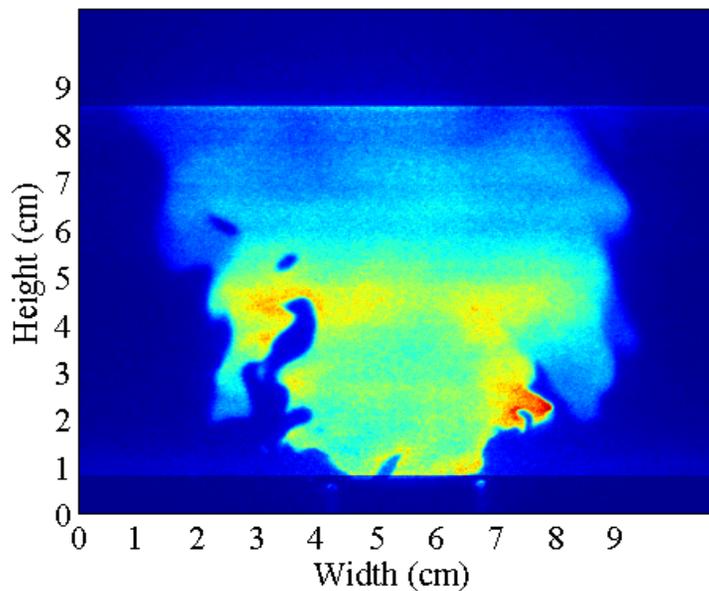
Flash back starts at 35s

Jet flame behavior starts 49s

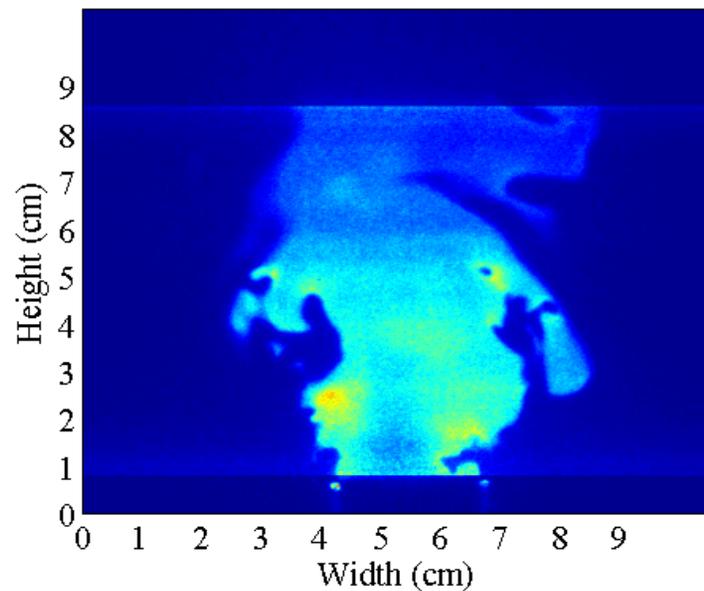
Flame extinction at 59s



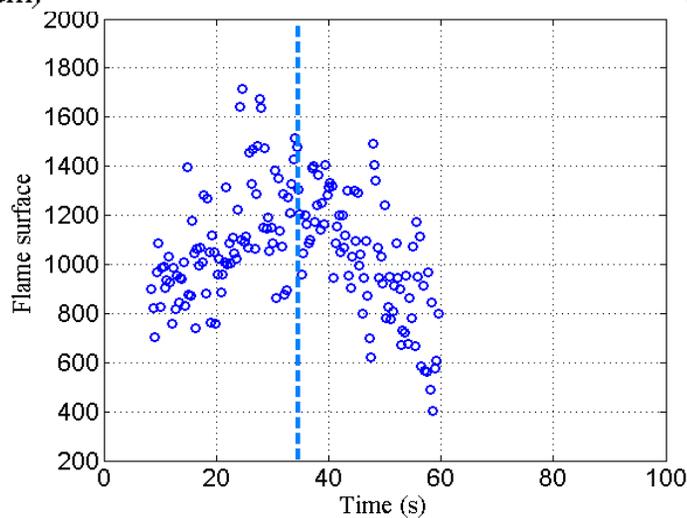
Flame Transition



Occasional Flash-back



Flame Anchored Upstream



Summary

- Flame Surface Density is constant across frequencies
- Guessing that the instability is driven by burner heating
- Increase in heat release appears to be driven by an increase in FSD
- If that is true, is the FSD increase driven by increasing turbulence intensity coming off of the swirler?
- Flash-back is probably driven by flow reversal driven by velocity oscillations at the burner exit
- Why does blowout occur?



Thanks for Listening!

Any Questions?



Analysis

Wave equation

$$\nabla^2 p' - \frac{1}{a^2} \frac{\partial^2 p'}{\partial t^2} = -\frac{1}{a^2} \frac{R}{C_v} \frac{\partial q'}{\partial t} + g$$

- Superscript ()' denotes deviations from mean value, a is the speed of sound, and the term g contains all influences other than that of heat addition.

Energy per cycle

$$\Delta \varepsilon_n(t) = (\gamma - 1) \frac{\omega_n^2}{E_n^2} \int dV \int_t^{t+\tau_n} \frac{p'_n}{\bar{p}} \frac{q'_n}{\bar{q}} dt$$

- n denotes different modes of the acoustic oscillation

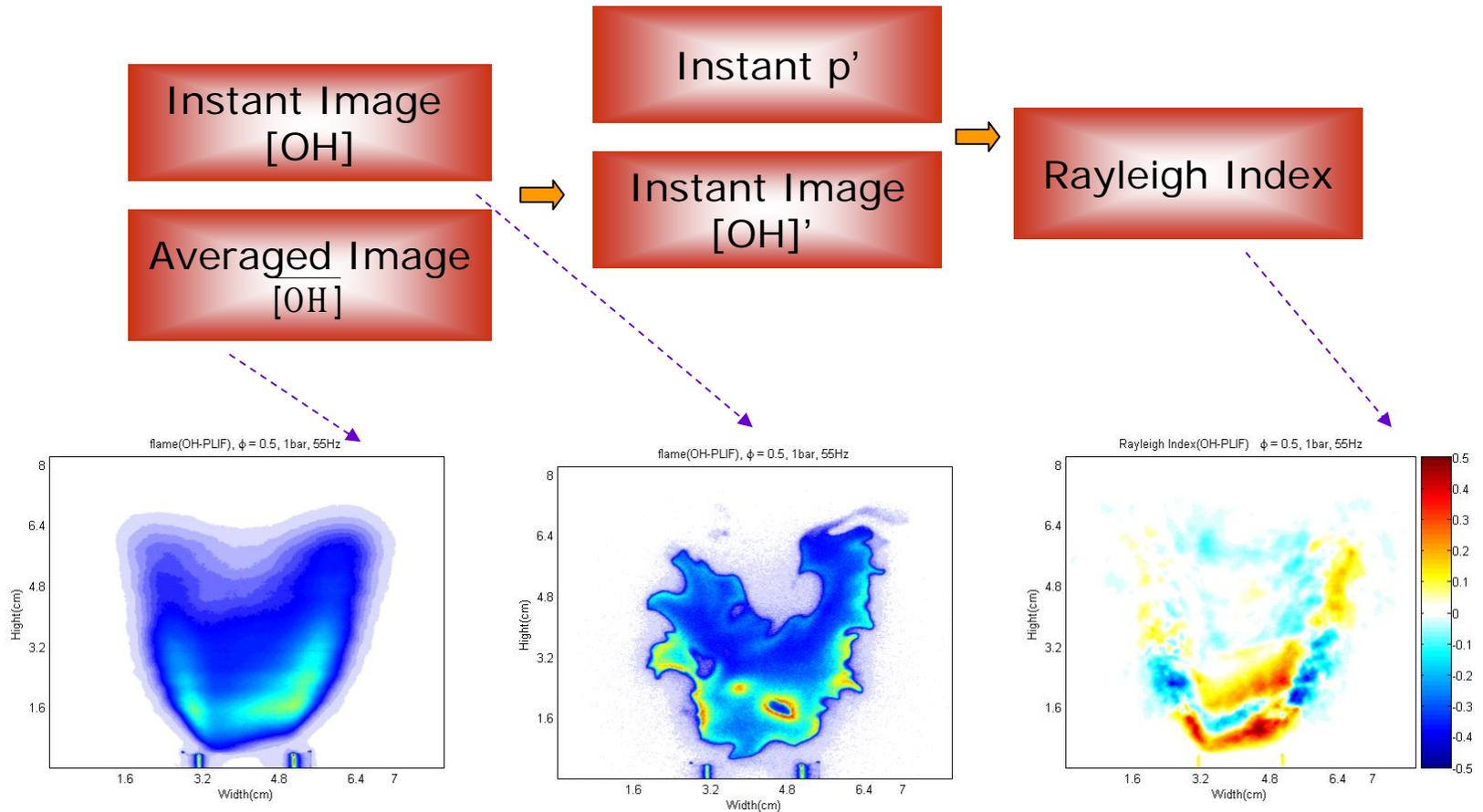
Rayleigh Index

$$R_f = \int_0^1 \frac{p' q'}{p_{rms} \bar{q}} d\xi$$

- Positive R_f means that pressure oscillation and heat release are in phase and hence the oscillation is enhanced
- In reality, a flame could be stable while exhibiting a positive Rayleigh Index since dissipation is not included in this equation



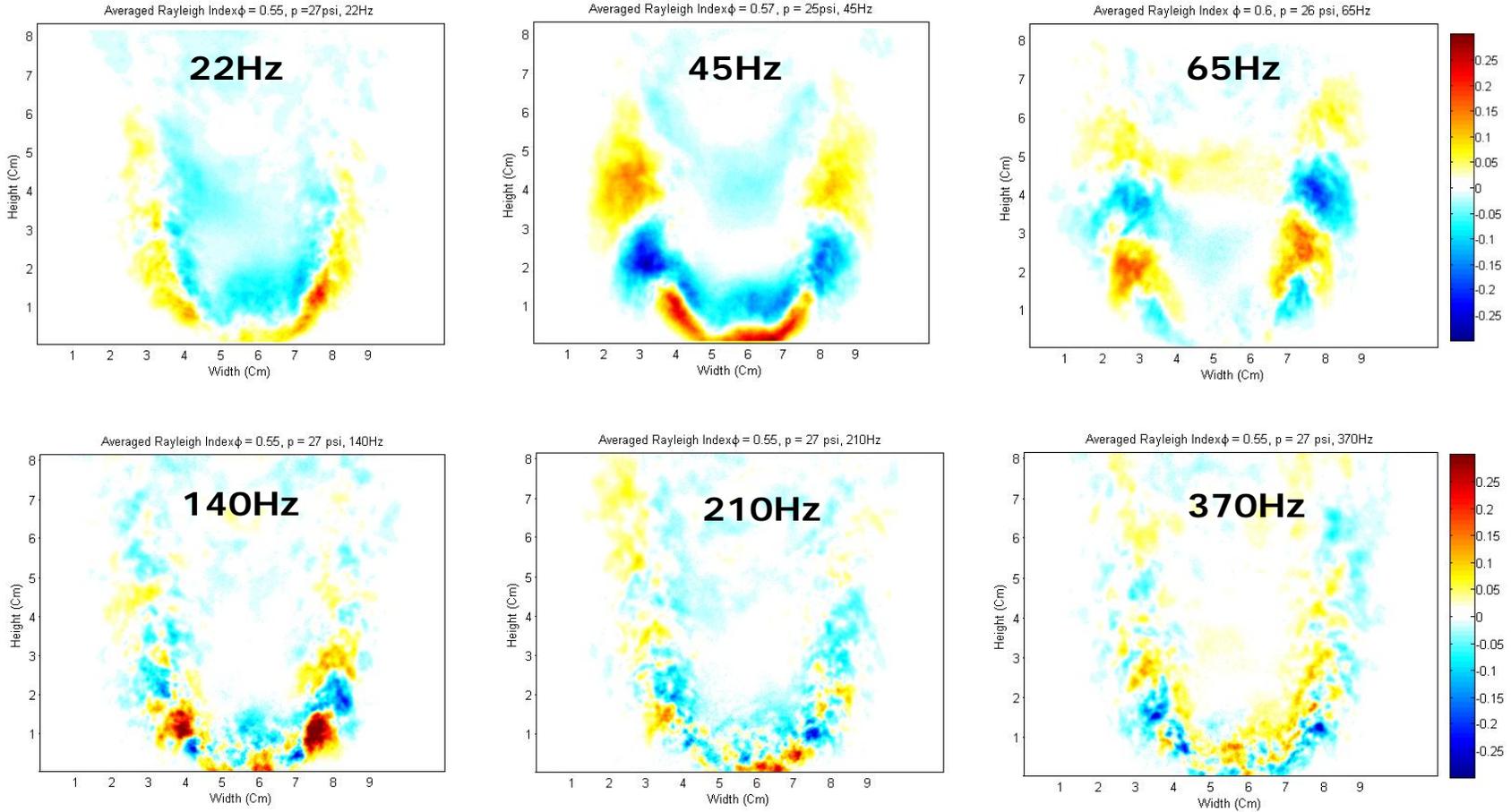
Data Reduction



- ❑ No clear structure seen from OH concentration
- ❑ Pattern appears in Rayleigh Index



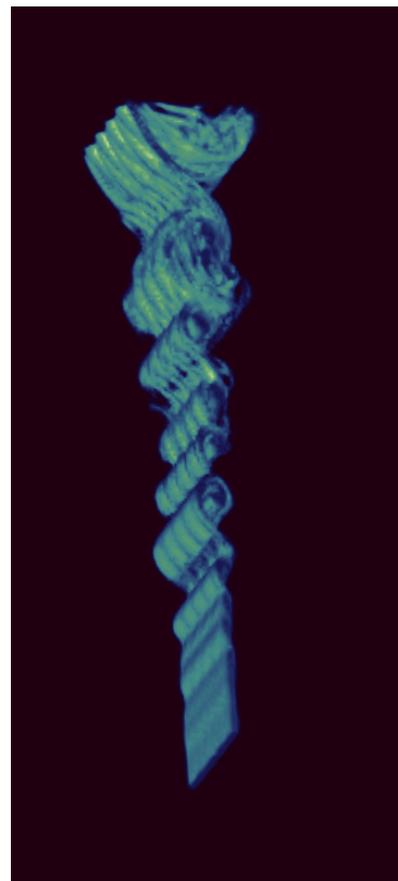
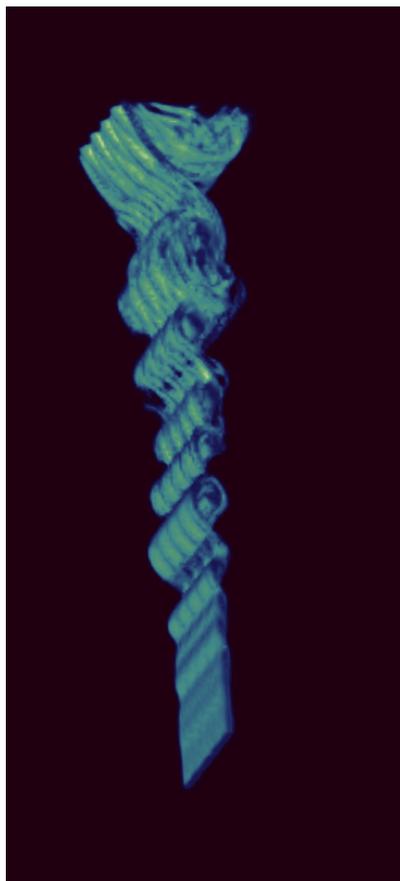
Rayleigh Index (1.8bar)



Rayleigh Index at elevated pressures



Shear Layer Forming Vortices

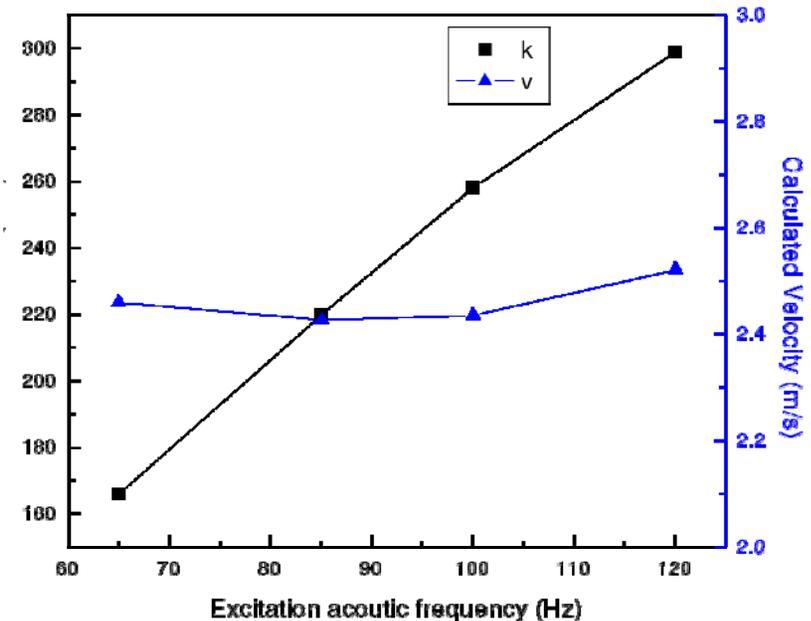
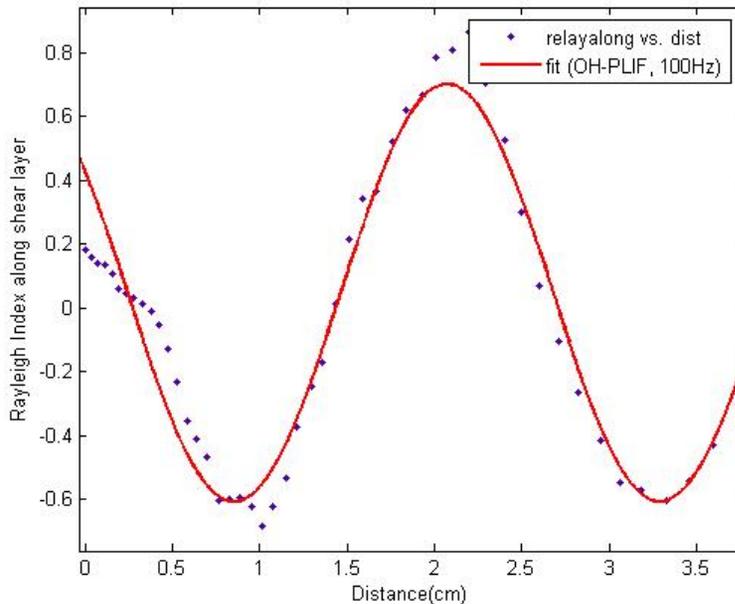


- A. S. Almgren, J. B. Bell, P. Colella, L. H. Howell, and M. L. Welcome, "A Conservative Adaptive Projection Method for the Variable Density Incompressible Navier-Stokes Equations," *J. Comp. Phys.*, **142**, pp. 1-46, 1998.



Vortex Behavior

- The Rayleigh Index through a line running between the vortex cores is extracted and a curve fit is applied



Rayleigh Index along the structure, 100Hz

Wave number and calculated velocity

$$k = \frac{2\pi}{\lambda} = 258$$

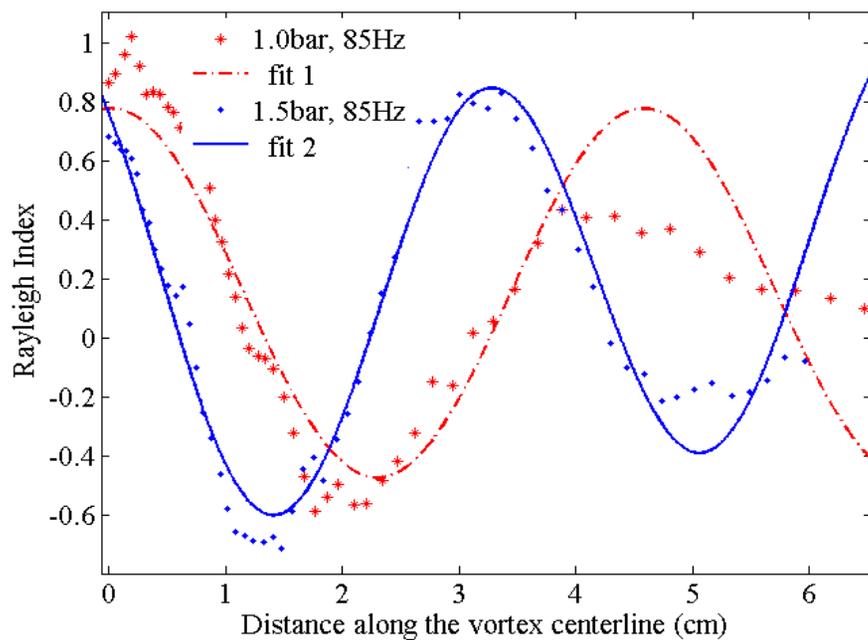
---Wave number

$$v = \frac{2\pi f}{k} = 2.43 \text{ m/s}$$

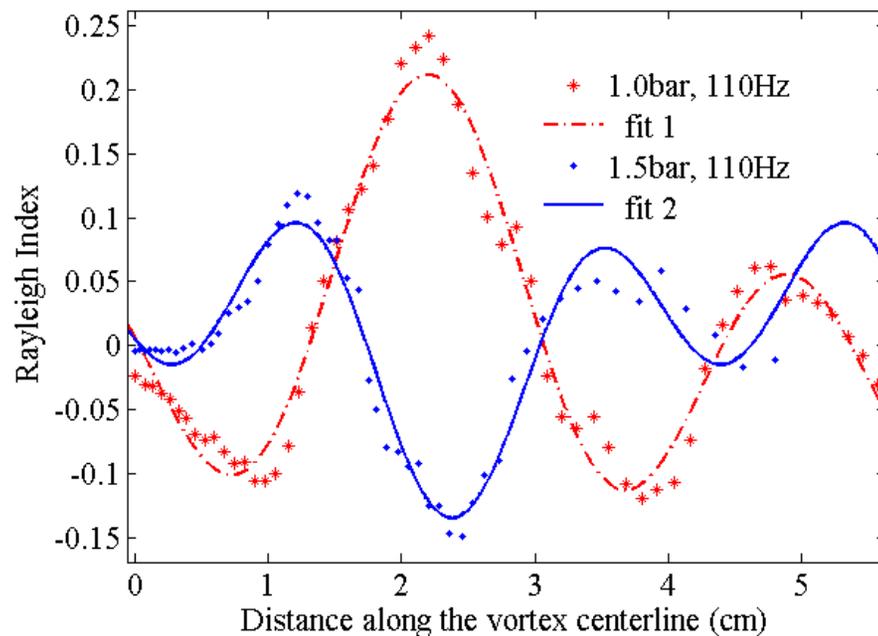
---comparable with the fluid velocity



Sensitivity to Swirl Number



Flame with swirl number of 0.5

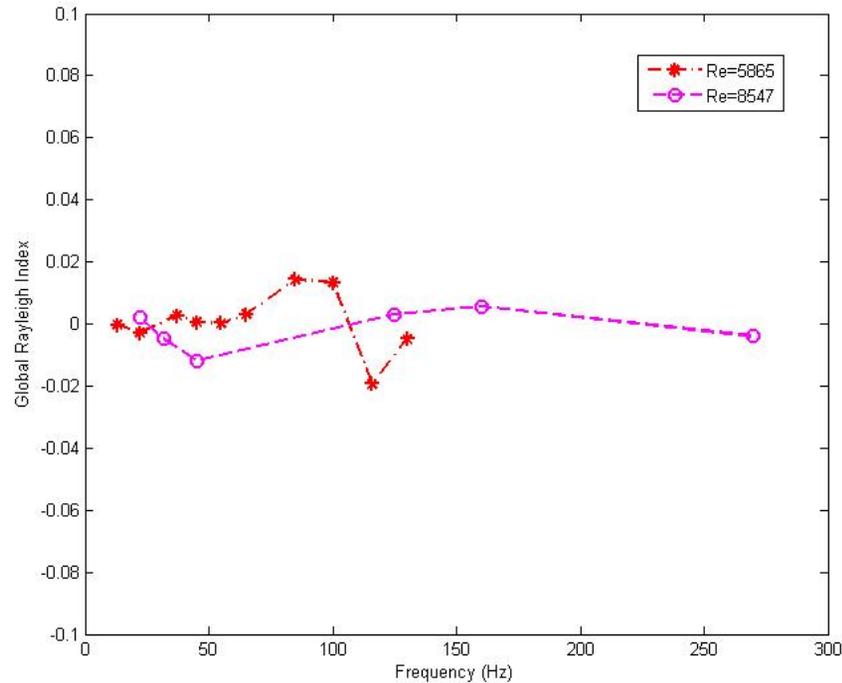


Flame with swirl number of 0.2

Neither swirl number nor pressure change have a significant impact on the coupling evident in these low swirl flames



Net Global Rayleigh Index



- Although there are local negative positive regions, the global Rayleigh index is close to zero
- Similar phenomena is observed for the other pressures tested
- The increase of pressure does affect the coupling but not significant difference observed yet



Coupling Range

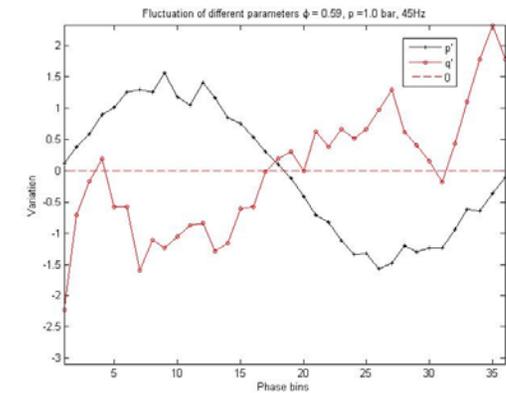
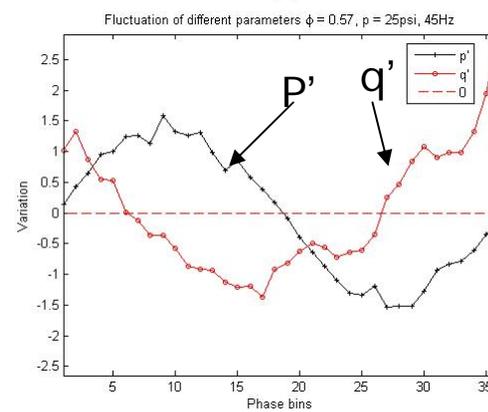
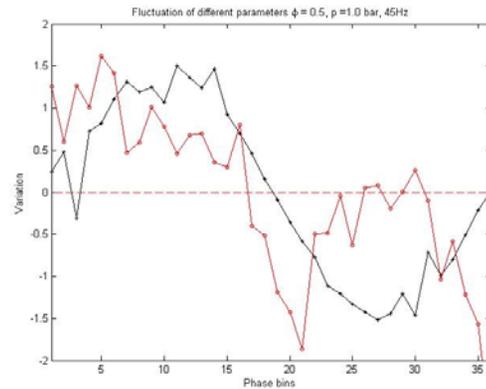
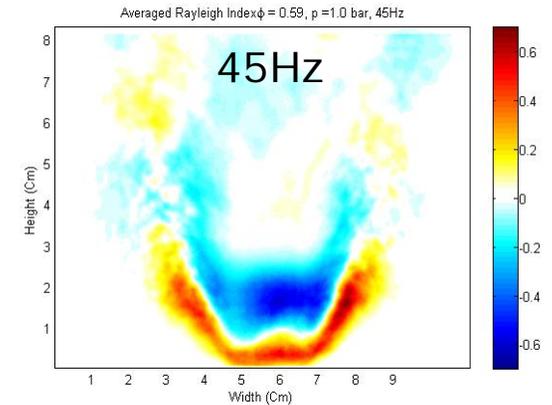
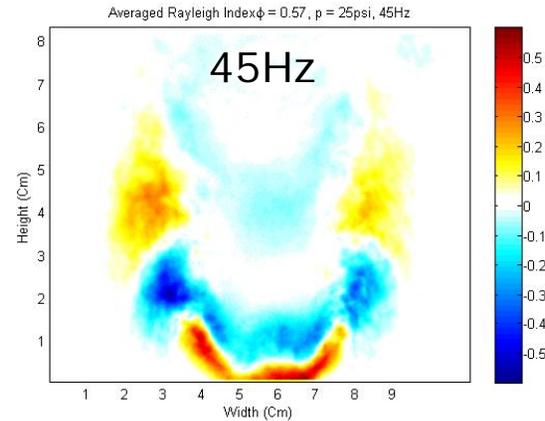
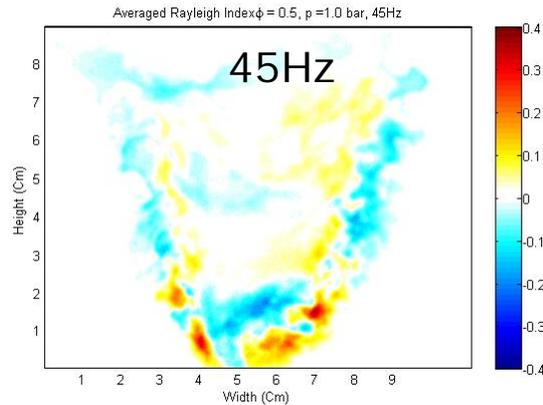
- How to predict the coupling?
 - Can you easily tie the shear layer instability to jet instability or behavior?
- Are Reynolds number and Strouhal number analyses useful?

$Re = UD \rho / \mu$	U is the inlet velocity
$St = fD / U$	D is the burner diameter
	f is excitation frequency
	μ is the dynamic viscosity of the reactants

- $Re = 5562$ (1bar), f : 55-120Hz, St: 0.27-0.87
- $Re = 7376$ (1.8bar), f : 22-140Hz, St: 0.23-1.49
- $Re = 8547$ (1bar), f : 22(tested), St: 0.11



Coupling range study



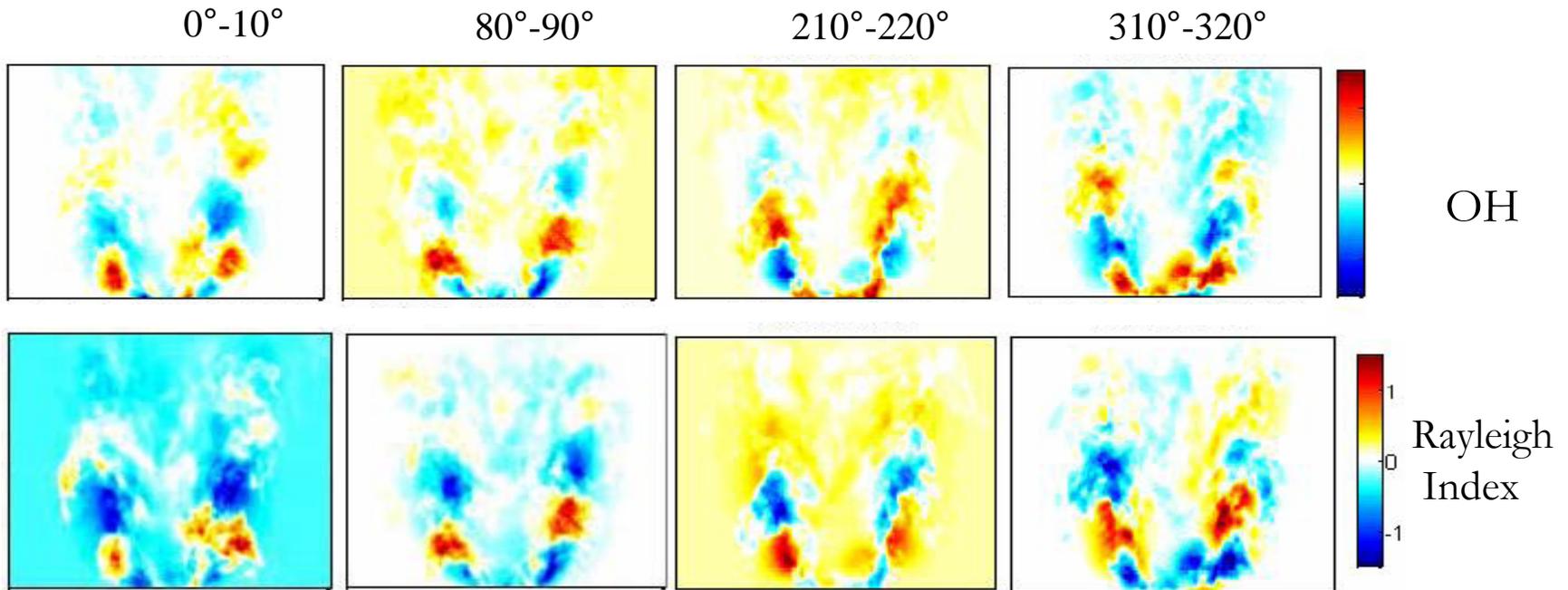
$Re = 5865$
 $U = 3.5$ m/s
 $St = 0.32$

$Re = 7040$
 $U = 2.05$ m/s (4.18 m/s at 1 bar)
 $St = 0.50$

$Re = 8547$
 $U = 5.18$ m/s
 $St = 0.20$



Rayleigh Index Exploration

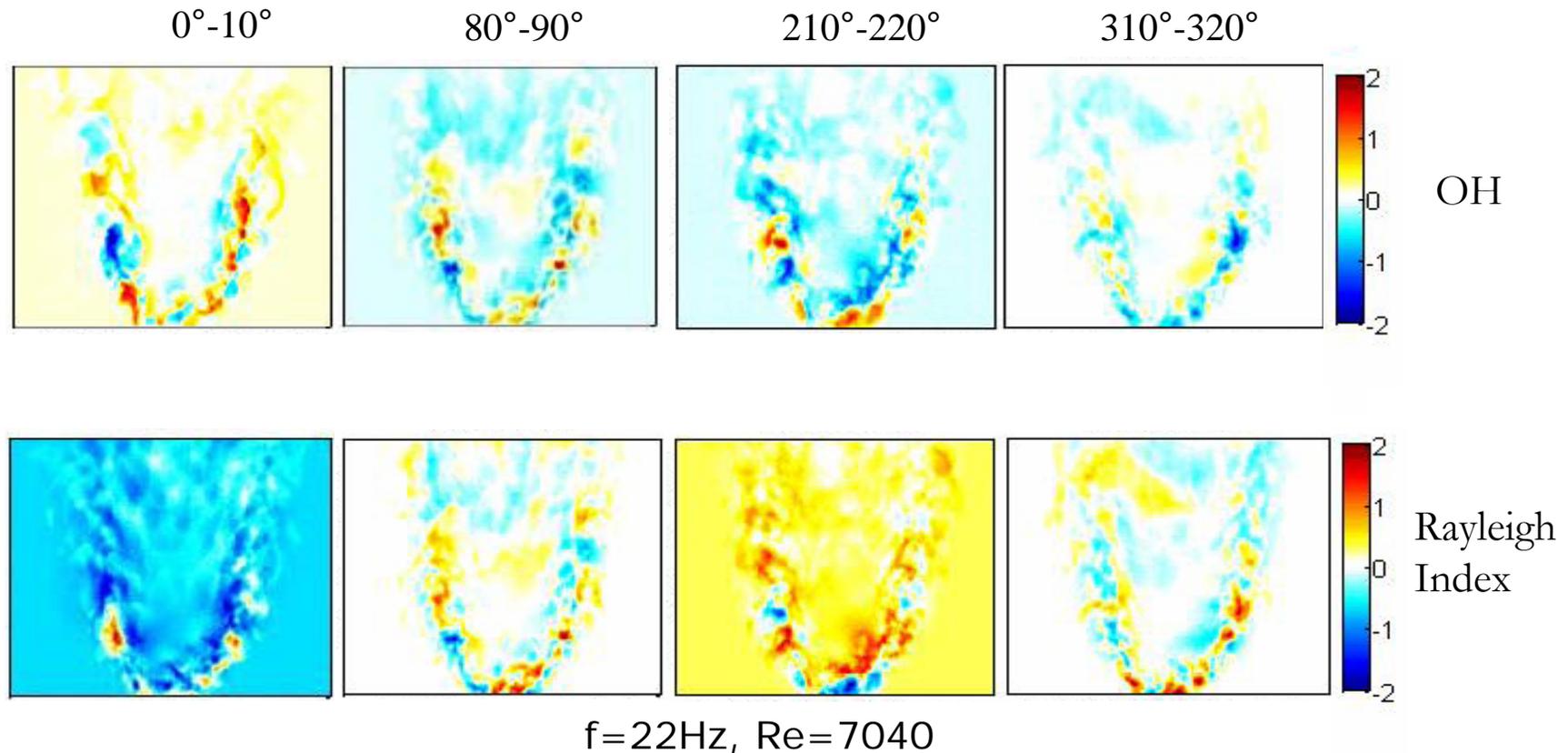


$f=116\text{Hz}$, $\text{Re}=7040$

- OH concentration changes in a cycle
- Rayleigh Index distribution doesn't change much in a cycle.



Comparison of Unstructured Flow



- When the acoustics perturbation and the shear layer are not coupled, there is no clear structures from OH and Rayleigh index.

